

A Methodology Document Detailing Biomethane Testing and Injection Pathways to Meet Existing Australian Standards and Regulatory Requirements

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RP3.2-09 Biomethane Impurities

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Abbreviations

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SUMMARY OF REPORT

This report aims to provide regulatory and technical information regarding biomethane injection into existing natural gas pipelines by undertaking two primary tasks:

- Reviewing state-by-state Acts, Laws and Regulations concerning quality requirements for natural gas transmission and distribution in Australia; and generating guidance on steps to be taken to facilitate biomethane injection in compliance with these regulations and with Australian Standard AS 4564.
- Performing computer-aided simulations to study natural gas and biomethane mixing under industrial conditions, track biomethane contaminants in natural gas pipelines and determine the mixing conditions that result in compliance with AS 4564 at the end user.

The review of state-by-state legislation identified clauses that relate to natural gas quality requirements. Wherever the legislation could be interpreted as allowing the extension of quality requirements to cases other than natural gas, guidance outputs detailing their applicability to biomethane injection have been produced. The guidance outputs identify the need for a new or amended safety and operating plan for biomethane-blended gas transport in existing natural gas pipelines. The amended plan is likely to include both feedstock and biomethane gas quality monitoring; as well as gas mixing studies that can predict the concentration of biomethane contaminants downstream of the injection point to ensure gas of AS4564 quality is delivered to end-use customers. The gas quality monitoring should be based on procedures and techniques already developed for biomethane promotion in other countries particularly for unconventional contaminants such as siloxanes. Computational Fluid Dynamics (CFD) simulations of biomethane and natural gas mixing show that a close to fully mixed flow can be achieved within a short distance from the injection point, resulting in uniform concentrations of contaminants at the point of end-use. Consequently, these concentrations can be estimated using mass balance calculations without requiring CFD simulations. Results showed compliant mixing was feasible for a range of biomethane compositions if natural gas concentrations were well within the compliance limits.

1 BACKGROUND

The promotion and use of renewable energy supplies like biomethane will play a pivotal role in decarbonizing and consolidating Australia's energy sector. Produced from biogas upgrading processes involving Carbon Dioxide (CO2) and Hydrogen Sulphide (H2S) removal, biomethane's major constituent is Methane (CH4), similar to natural gas, giving it the potential for being blended into existing natural gas grids and eliminating the need for the construction of independent biomethane transmission and distribution infrastructure. However, depending upon the source from which the biomethane is produced, it may contain contaminants that are not present in natural gas. A previous literature review on biomethane impurities revealed that the contaminants of concern are either similar to those found in natural gas (such as Oxygen (O_2)) but at elevated concentrations; or can be classified as "unconventional" and specific to the feedstock from which the biomethane is derived [1]. These unconventional contaminants can include siloxanes, ammonia, halocarbons and volatile organic compounds. The literature review analysed regulatory requirements in over 18 different biomethane-producing jurisdictions and proposed limit values for the concentrations of unconventional contaminants in natural gas pipelines that can be adopted by Australian decision-makers to facilitate biomethane injection. Equally importantly, the literature review concluded that no changes are required for most of the quality parameters mandated by AS 4564 (e.g. higher heating value (HHV),

hydrocarbon dew point and hydrogen sulphide content). However, there would be concerns about maximum allowable O_2 and inert gas (primarily Nitrogen (N_2) and CO_2) concentrations due to their elevated levels in biomethane, relative to natural gas. The current AS 4564 limit for O₂ is 0.2 mol% but studies show its concentration within biomethane can reach up to 2 mol% [2]. Bringing O₂ levels down to the AS 4564 limit is not always viable from the biomethane producers' perspective due to significant additional costs [3]. Similarly, studies show that the inert gas content in the biomethane derived from landfill gases can be up to 10 mol% against 7 mol% as the maximum allowable limit in AS 4564 [3]. Since the Wobbe Index (WI) is intrinsically tied to the concentration of inert gases, there is also concern about the lower WI limit. As a result, work is required to create quality standards and/or safety and operating plans based on Australian legislation to ensure that no adverse impacts from biomethane impurities are imposed on both pipeline owners/operators and end-point customers.

This report is focused on the creation of a methodology document for biomethane injection into the Australian natural gas network based on:

- Gas quality compliance requirements from state-by-state legislation associated with natural gas transport in pipelines.
- Guidance outputs derived from the state-by-state legislation outlining safety and operational requirements for natural gas flow in pipelines that can be extended to biomethane injection.
- Computational Fluid Dynamics (CFD) studies investigating the effectiveness of natural gas and biomethane mixing to determine conditions that result in AS 4564 compliant gas at the end-user, as a function of the concentration of O_2 and inert gases in the feed biomethane, as well as biomethane and natural gas flowrates.

Excluded from this report are:

- The possibility of changes to AS 4564 limits for O₂ and inert gases, as well as lower WI index. Project RP1.4-07 is currently studying the influence of increased $O₂$ and inert gas concentrations on end-user appliances. Similarly, Milestone 5 of this project will complete a desktop review and corrosion modelling for integrity-based impacts of raising AS-4564 oxygen limits on Australian natural gas networks. Only after these two projects have been completed will there be sufficient evidence to consider the possibility of changes to AS 4564.
- Mixing studies on the influence of unconventional contaminants (e.g. siloxanes and ammonia, etc.) on the final composition of the blended gas delivered to customers.

2 TARGETED REGULATIONS

Project RP1.2-04 has recently identified viable locations for biomethane production and injection in natural gas pipelines [4]. The locations are primarily based in the states of Victoria (VIC), New South Wales (NSW), Queensland (QLD) and Southern Australia. Hence, natural gas regulations of these states were studied in the present project. Presented in Table 1 are the targeted regulations alongside their objectives in the framework of natural gas quality requirements.

Table 1. Objectives of state-by-state Laws, Acts and Regulations in the framework of safety and quality requirements for natural gas transmission and distribution

3 GUIDANCE OUTPUTS

Relevant text from the above Acts, Laws and Regulations is provided in Appendix A. Guidance outputs generated from this text is provided in Table 2. In summary, the potential pathways to compliant biomethane injection is to seek exemptions from the current legislation and to create new or amended safety and operating plans containing measures in place to ensure the safety of the gas for both pipeline operators and end-users.

Table 2. Guidance outputs for biomethane injection derived from legislation

4 LIKELY COMPONENTS OF AMENDED SAFETY AND OPERATING PLANS

An amended safety and operation plan is likely to include:

Risk Assessment: A risk assessment will consider:

- The flowrate of biomethane to be injected into the transmission or distribution network, relative to the natural gas flowrate. A smaller proportion of biomethane relative to the total flow is lower risk and will require less additional monitoring.
- The duration of the biomethane injection. A short-term trial is likely to have less effect on pipeline and enduser appliance integrity than a permanent installation.
- The pipeline length between the injection point and the end user. A longer length ensures complete mixing of the gas supplies (see Section 5).
- The source of the biomethane supply. For example, biogas derived from agricultural waste such as dairy waste is highly unlikely to contain siloxanes or halogenated compounds, so monitoring of these potential contaminant should not be required [1]. Similarly, only landfill derived gas contains significant concentrations of ammonia, hydrogen sulphide and carbon monoxide. Refer to Milestone Report 2 (Literature Review) Tables 4 and 46 [1].
- Quantitative composition data for both the biogas and biomethane, based on initial pilot plant or laboratory trials. Alternatively, pre-injection testing over a period of some weeks may be needed before acceptance by the grid operator[5].
- The processes used to upgrade the biogas into biomethane, as some are more effective than others in reducing specific contaminant concentrations. Refer to Milestone Report 2 (Literature Review) Table 8 [1].
- Quantitative composition data for the underlying natural gas, particularly any residual water vapor concentrations. A combination of elevated water concentrations in the natural gas, with high oxygen concentrations in the biomethane could lead to elevated pipeline corrosion rates. This will be the subject of our Milestone 5 report.

Biomethane Feedstock Monitoring: It will often be easier to monitor contaminants as they occur in the raw biogas or the raw biomass feedstock, rather than the upgraded biomethane, due to the higher concentrations. Typical biogas concentrations for a range of contaminants and the corresponding biomethane concentrations are provided in Milestone Report 2 (Literature Review) Tables 28 - 41 [1]

Biomethane Quality Monitoring: Standard attributes that already have existing limit values in AS 4564 (such as total inert concentration and heating value) should be continuously monitored at the point of biomethane injection using the procedures developed for standard natural gas. This is commonly Gas Chromatography (GC) analysis with a Thermal Conductivity Detector (TCD) following ASTM D1945/1946 [6]. Other potential contaminants without existing limit values in AS 4564 (e.g. siloxanes) can be monitored by taking quarterly or annual samples of the gas for testing by an independent certified third-party laboratory [5], particularly if feedstock monitoring is also in place. Refer to Milestone Report 2 (Literature Review) Table 12 [1] for potential testing methods.

Gas Quality Monitoring Downstream of Injection Point: Standard attributes that already have existing limit values in AS 4564 should be continuously monitored using established procedures at a suitable point at least 50m downstream of injection to confirm mixing of natural gas and biomethane is complete.

Outcomes of research studies on biomethane and natural gas mixing: The mixing of biomethane and natural gas may result in a gas non-compliant with AS 4564 due to the elevated concentrations of O_2 and N₂. Computational Fluid Dynamics (CFD) simulations can provide three-dimensional concentration distributions of individual contaminants downstream of injection. This can determine what biomethane compositions can be injected into natural gas pipelines to be AS 4564 compliant gas upon reaching end-users. See Section 5 below for typical simulations.

5 CFD SIMULATIONS OF NATURAL GAS AND BIOMETHANE MIXING

5.1 Simulation Details

The basis for our CFD simulations are provided in Table 3. The temperature and pressure of the simulations are typical of underground natural gas transmission pipelines. Natural gas is assumed to be limited to the components shown in Table 3, even though it can contain other minor components not listed here. The concentrations of $O₂$ and inert gases (N_2 plus CO_2) were set to their maximum limit values in AS 4564, 0.2 mol% and 7 mol%, respectively, as no reference composition for natural gas in Australian pipelines was found. This natural gas composition represents an extreme case where the concentrations of O₂ and inert gases are likely much greater than their typical values. Similarly, biomethane composition was intentionally varied in a way to allow for the introduction of very high levels of contaminants to the natural gas pipelines. As a result, the mixing studies consider "worst-case" scenarios where the concentrations of the contaminants in natural gas pipelines are probably more than the concentrations under industrial conditions.

Table 3. CFD simulation basis for biomethane and natural gas mixing studies

5.2 Simulation Results

Typical O² compositions after biomethane and natural gas blending is shown in Figure 1. Two pipeline lengths of 20 m and 40 m were used for the simulations with the biomethane composition set to 8 mol% N_2 , 2 mol% O_2 and 2 mol% $CO₂$. The natural gas flowrate is 8600 STD m³/h (165 actual m³/h) while the biomethane flowrate is 1600 STD m^3/h (30 actual m^3/h) giving a ratio of biomethane to natural gas flow of 0.18. Results show a close to fully mixed flow within relatively short distances from the injection point, representing insignificant changes in contaminant concentrations within the natural gas pipeline.

Figure 1. The mole fraction of O_2 in natural gas pipeline after blending with biomethane. Top and bottom contours represent simulation results for pipelines of 20 m and 40 m, respectively. The biomethane contained 2 mol% oxygen and the ratio of biomethane to natural gas flow was 0.18.

To better visualize the extent of mixing, Figure 2 shows a comparison of the oxygen mol fraction at the upper edge of the pipe versus the average value at different locations within the pipeline. The two mole fractions converge with less than 5% difference both in radial and axial directions after 20 m, as the flow becomes close to fully mixed downstream of the injection point. Achieving a fully mixed flow within a short distance from the injection point is the major outcome of these CFD studies, as it ensures the gas delivered to end-use customers will have consistent specifications.

Another simulation considered the blending of the same proportion of raw biogas into natural gas (i.e. a ratio of 0.18 and a total flowrate of 10,200 STD m³h). A biogas composition of 50 mol% N₂, 10 mol% O₂ and balance CH₄ was chosen in order to simulate worst-case conditions. Again, a close to fully-mixed flow is achieved within a short distance from the injection point (Figure 3). The average and upper edge concentrations are again close to identical within 20 m of the mixing point, even though the biogas is significantly different in composition (Figure 4).

Figure 2. Upper edge versus average mole fractions of $O₂$ as a function of pipeline length. Note the difference in scale used in the inset spheres. The biomethane contained 2 mol% oxygen. The natural gas flowrate is 8600 STD m3/h while the biomethane flowrate is 1600 STD m3/h, giving a ratio of biomethane to natural gas flow of 0.18.

Figure 3. The mole fraction of O_2 in a 40 m natural gas pipeline after blending with a raw biogas composed of 50 mol% N2, 10 mol% O² and CH⁴ balanced. The natural gas flowrate is 8600 STD m3/h while the biogas flowrate is 1600 STD m3/h, giving a ratio of biogas to natural gas flow of 0.18.

Figure 4. Upper edge versus average mole fractions of O_2 and N_2 as a function of pipeline length when blending raw biogas and natural gas. The raw biogas contains 50 mol% N₂, 10 mol% O₂ and CH₄ balanced. The natural gas flowrate is 8600 STD m3/h while the biogas flowrate is 1600 STD m3/h, giving a ratio of biogas to natural gas flow of 0.18.

Biomethane composition and flowrate, as well as natural gas flowrate were varied to investigate whether the fully mixed flow conclusion remains valid under various operating conditions. The average and upper edge concentrations continue to converge at a pipeline length of 20m as shown in Figures 5-7.

Figure 5. Effect of $O₂$ and inert gas concentrations in biomethane on the final mixed gas concentrations in a pipeline of length 20 m. Biomethane to natural gas flowrate was fixed at a ratio of 0.18. Other simulation details are listed in Table 3.

Figure 6. Effect of biomethane flowrate on the final mixed gas concentrations in the pipeline of length 20 m. Biomethane composition is set to 8 mol% N₂, 2 mol% O₂, 2 mol% CO₂ and CH₄ balanced. Other simulation details are listed in Table 3.

Figure 7. Effect of natural gas flowrate on the final mixed gas concentrations in the pipeline of length 20 m. Biomethane composition is set to 8 mol% N₂, 2 mol% O₂, 2 mol% CO₂ and CH₄ balanced. Other simulation details are listed in Table 3.

In all simulations, the final mixed gas concentrations exceeded the limit values mandated by AS 4564 because the maximum allowable concentrations of O_2 and inert gases were assumed as a starting point. Typical pipeline concentrations are likely much lower than the maximum limit values which would result in the mixed gas being compliant with AS 4564.

The results indicate that in all cases, performing CFD simulations is not necessarily required with the average mixture concentration calculated from a mass balance sufficient to calculate the composition of the blended gas, if more than 40m from the point of injection. If the calculated mixed gas concentration is within the limit values of AS 4564, then it can be injected into the natural gas pipeline.

6 CASE STUDIES OF GAS MIXING COMPLIANT WITH AS 4564

The aim of this section is to show under which conditions the mixing of biomethane with natural gas would be compliant with AS 4564. Based on the outcome of CFD simulations, simple mass balances are sufficient for this purpose, if injection is more than 40 m upstream of the end user. For these calculations, it was assumed that the natural gas was a binary mixture of 0.05-0.2 mol% O₂ with balance CH₄ which was mixed with a biomethane stream consisted of 1-3 mol% O_2 and balance CH₄. The mole fraction of O_2 is plotted as a function of the biomethane to natural gas flowrate in Figure 8, with the area of compliance with AS 4564 (i.e. maximum 0.2 mol% O₂) highlighted. At 0.05 mol% O_2 in natural gas and 1 mol% O_2 in biomethane, blending would be compliant if the ratio of biomethane to natural gas flowrate was set to 0.2 or less. When increasing the biomethane concentration of O₂ to 2 mol%, the biomethane flowrate should be ≤ 10% of the natural gas flowrate to have a compliant mixed gas. The area of compliant mixed gas becomes smaller when the natural gas contains 0.1 mol% O₂, with a ratio of 0.12 biomethane to natural gas flowrate needed for biomethane containing 1 mol% O₂. Figure 8 also shows compliant blending with O_2 levels greater than 1 mol% in biomethane. For instance, if the natural gas and biomethane concentrations of O_2 were set to 0.1 mol% and 2 mol%, the compliant blending would occur at biomethane to natural gas flowrate ratios of 0.06 or less.

Figure 8. Mixing of natural gas and biomethane composed of binary mixtures of $O₂$ and CH₄. The red dashed line represents the threshold below which gas mixing compliant with AS 4564 can be achieved.

Mixing calculations for binary mixtures of N_2 as representative of the total inert gas concentration and CH₄ were undertaken. The natural gas concentrations of N₂ were set to 5 mol% and 6.5 mol% (CH₄ balanced). The concentration of N² in biomethane was varied from 8 to 10 mol% (CH⁴ balance) (Figure 9). Injecting biomethane with 8 mol% N₂ into natural gas with 6.5 mol% N₂ would give a compliant mixed gas at a biomethane to natural gas flowrate ratio of < 42%. Compliance would also be achieved with 9 and 10 mol% N² in biomethane at the same natural gas composition, but lower flowrate ratios. Reducing the natural gas concentration of N_2 to 5 mol% would result in compliant mixed gas at all biomethane to natural gas flowrate ratios used in these simulations. Wobbe Index would also lie above the minimum value of AS 4564 for all conditions tested with 5 mol% N_2 in the natural gas (Figure 10) but only some flowrate ratios for 6.5 mol% N_2 in the natural gas supply.

Figure 9. Mixing of natural gas and biomethane composed of binary mixtures of N₂ and CH₄. The red dashed line represents the threshold below which gas mixing compliant with AS 4564 would be achieved.

Figure 10. Mixing of natural gas and biomethane composed of binary mixtures of N₂ and CH₄. The red dashed line represents the threshold above which gas mixing compliant with AS 4564 would be achieved.

7 CONCLUSIONS

Major conclusions from this work include:

- Existing state-by-state legislation contains regulatory requirements that can be extended to biomethane injection into natural gas grids. A potential pathway that may enable biomethane injection are through **seeking exemption from authorities and amending safety and operating plans and safety management systems** for pipeline operation.
- An amended safety and operating plan may be comprised of **risk assessment**, **biomethane feedstock monitoring, biomethane gas quality monitoring, downstream gas quality monitoring** and **outputs from CFD studies** on biomethane blending into natural gas.
- \triangleright The major outcome of the CFD studies presented here is that the biomethane-blended natural gas becomes close to **fully mixed within 20 m from the injection point**, with less than 5% change in the concentrations of the gas constituents compared to the average. This means that if the average composition of the mixture is within AS 4564 limits, this should be delivered to end-users further away. Results also confirmed that close to fully-mixed flow is also achieved when a raw biogas composed of large quantities of contaminants is mixed with the natural gas.
- \triangleright Knowing that the mixing of biomethane and natural gas would become fully mixed upon reaching end-use customers, mass balance calculations can be used to estimate the final specification of the mixed gas. Calculations show that compliant blending should be possible in many circumstances.

8 REFERENCES

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APPENDIX A: RELEVANT TEXT FROM GAS QUALITY REGULATIONS

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